

# Hydrogenation of Benzaldehyde and Cinnamaldehyde in Compressed CO<sub>2</sub> Medium with a Pt/C Catalyst: A Study on Molecular Interactions and Pressure Effects

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The hydrogenation of benzaldehyde and cinnamaldehyde has been studied with a 5% Pt/C catalyst in compressed CO<sub>2</sub>. The effect of CO<sub>2</sub> pressure on the total conversion was found to be different between the two aldehydes. The total conversion of benzaldehyde merely decreases with increasing CO<sub>2</sub> pressure, while that of cinnamaldehyde shows a maximum at a certain pressure. High-pressure FTIR measurements indicate the existence of interactions of CO<sub>2</sub> with the aldehydes. The absorption of  $\nu(\text{C}=\text{O})$  red-shifts at increasing CO<sub>2</sub> pressure, and this red-shift is more significant for cinnamaldehyde than for benzaldehyde, indicating that the C=O bond of the former becomes more reactive than the latter. The difference in the mode of interactions of CO<sub>2</sub> with these aldehydes has also been indicated by changes of  $\nu(\text{C}=\text{O})$  of CO<sub>2</sub>. Thus, the conversion of benzaldehyde will decrease with increasing CO<sub>2</sub> pressure because of a simple dilution by introducing a larger quantity of CO<sub>2</sub>. For cinnamaldehyde, the conversion will increase at low pressures because of increasing interactions with CO<sub>2</sub> molecules (increasing the reactivity of the C=O bond) but decrease at high pressures because of the simple dilution effect, similar to the case of benzaldehyde. The dense CO<sub>2</sub> molecules are not likely to change the catalytic activity of supported Pt particles, which was previously suggested from optical absorption of supported fine metal (Au) particles in a compressed CO<sub>2</sub> medium.

## 1. Introduction

Hydrogenation of organic compounds is an industrially important chemical transformation. Gaseous H<sub>2</sub> is an inexpensive and versatile reagent for hydrogenation, but the rate of hydrogenation is usually slow, because H<sub>2</sub> is less soluble in common organic solvents. By contrast, supercritical carbon dioxide (scCO<sub>2</sub>) is completely miscible with H<sub>2</sub>, and it is an environmentally benign medium with good mass and thermal transport properties.<sup>1–4</sup> So, the use of scCO<sub>2</sub> has been attracting much attention for developing green chemistry processes. Hydrogenation is one of the frequently studied reactions in scCO<sub>2</sub> using homogeneous<sup>5–9</sup> and heterogeneous catalysts.<sup>10–20</sup> Practical merits of the use of heterogeneous catalysts include ease of separation, recovery, and recycling.

It is known for hydrogenation as well as other reactions in scCO<sub>2</sub> that the CO<sub>2</sub> pressure often significantly affects the total conversion and product distribution in different manners depending on the reaction conditions. In most cases reported so far, the enhancement of the rate of catalytic hydrogenation of organic substrates in scCO<sub>2</sub> has been ascribed to high H<sub>2</sub> concentration in the liquid or gas phase in which the substrates and catalysts exist and/or to the elimination of mass transfer resistance due to complete miscibility of CO<sub>2</sub> and other reacting species. For example, Phiong et al. observed that scCO<sub>2</sub> significantly enhances the rate of  $\alpha$ -methylstyrene hydrogenation with 1% Pd/C under three-phase conditions.<sup>10</sup> Tschan et al. indicated the importance of phase behavior in continuous semi-hydrogenation of phenylacetylene to styrene with a Pd<sub>81</sub>Si<sub>19</sub>

alloy. They showed that a single-phase mixture at low H<sub>2</sub> pressure is an ideal medium for this semi-hydrogenation. The hydrogenation in scCO<sub>2</sub> has also been studied in our laboratory using heterogeneous catalysts as well as homogeneous ones. Significant enhancement in activity and selectivity was shown for the hydrogenation of unsaturated aldehydes with supported transition-metal catalysts in scCO<sub>2</sub>.<sup>12–16</sup> The above-mentioned effects of scCO<sub>2</sub> are also important for these hydrogenation reactions. In addition, we previously suggested the possibility that dense CO<sub>2</sub> changes the properties of supported metal particles. This was assumed from optical absorption measurements of small Au particles in dense CO<sub>2</sub> medium,<sup>21</sup> and this idea was invoked to explain the change of product distribution in Pt-catalyzed nitrobenzene hydrogenation with CO<sub>2</sub> pressure.<sup>13,14</sup> Furthermore, the coordination of CO<sub>2</sub> with active metal centers has been thoroughly reviewed.<sup>22,23</sup> It is indicated that only a weak interaction between CO<sub>2</sub> and an active metal center is sufficient to bring about insertion of CO<sub>2</sub> into an M–X bond (M = metal), which could modify the catalytic activity of this metal in dense CO<sub>2</sub>.

Recently, IR spectroscopy has been used to study the mixture of organic compounds in dense CO<sub>2</sub> at different pressures. In a CO<sub>2</sub> molecule, the carbon atom is partially positive and the oxygen atoms are partially negative, and this polar nature is significant in compressed CO<sub>2</sub>. Hyatt et al.<sup>24</sup> measured IR spectra of several probe compounds in both liquid and supercritical CO<sub>2</sub>. They reported that red-shifts in the  $\nu(\text{C}=\text{O})$  of acetone and cyclohexanone in dense CO<sub>2</sub> were slightly greater than that in *n*-hexane but slightly smaller than those in aromatic solvents, which show a tendency for CO<sub>2</sub> to interact with basic carbonyl groups. Brokeman et al.<sup>25</sup> suggested that the specific interaction between CO<sub>2</sub> and carbonyl oxygen could be de-

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scribed as a Lewis acid–base reaction. Such molecular interactions have been investigated further by Raveendran et al.,<sup>26</sup> who indicated the interaction of CO<sub>2</sub> molecules with Lewis base groups, especially carbonyl groups, through a C–H···O hydrogen bond with the hydrogen atom attached to the carbonyl carbon or at the  $\alpha$ -position. These interactions with CO<sub>2</sub> were suggested to affect the solubility of the substrate and the phase behavior of the reaction mixture in CO<sub>2</sub>, changing the chemical reactions in dense CO<sub>2</sub>. Recently, the application of various in situ spectroscopic techniques for the investigation of mixtures in supercritical fluids has been reviewed extensively.<sup>27</sup>

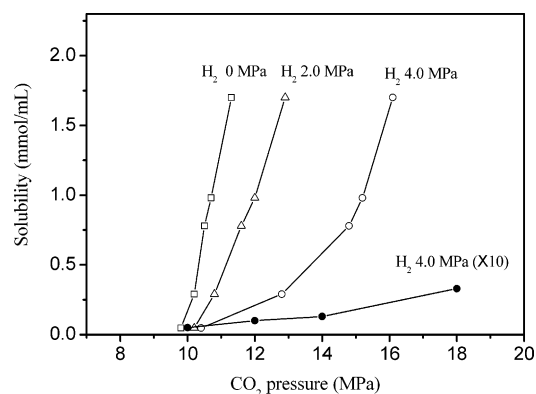
Although a number of homogeneously and heterogeneously catalytic reactions have been investigated in scCO<sub>2</sub>, fundamental studies at molecular levels are still insufficient to understand the CO<sub>2</sub> pressure effects on catalytic and noncatalytic reactions in scCO<sub>2</sub>. The present work has been undertaken to study in detail the CO<sub>2</sub> pressure effects in hydrogenation of two aldehydes, benzaldehyde and *trans*-cinnamaldehyde, with a Pt/C catalyst. It has been observed that the change of conversion with CO<sub>2</sub> pressure is significantly different between these two aldehydes. Other physicochemical measurements have been made to examine the effects of dense CO<sub>2</sub> medium observed, and the hydrogenation results have been discussed in terms of phase behavior, molecular interactions with CO<sub>2</sub> molecules (measured by in situ high-pressure FTIR), and change of the catalytic activity of Pt particles.

## 2. Experimental Section

**2.1. Materials.** All chemicals were purchased from Wako and used without further purification. A 5 wt. % Pt/C catalyst also purchased from Wako was reduced by hydrogen at 300 °C for 2 h before activity measurements. The size of the Pt particles obtained was examined by X-ray diffraction (XRD) and transmission electron microscopy (TEM) measurements and determined to be 8.3 nm, which gave a degree of metal dispersion of 0.11 from an approximate expression: metal dispersion = 0.9/diameter (in nm).<sup>28</sup>

**2.2. Phase Behavior and Solubility.** The examination of the phase behavior is important to study chemical reactions in scCO<sub>2</sub>; it is significant to see whether the reaction is taking place homogeneously in a single phase or heterogeneously in two or more phases. A 10 cm<sup>3</sup> high-pressure sapphire-windowed view cell was used to determine the separate pressure from a two-phase (gas–liquid) state to a one-phase (scCO<sub>2</sub>) state and estimate the solubility of the substrate in scCO<sub>2</sub>. A certain amount of substrate was added into the cell, and then, the cell was flushed with 0.5 MPa CO<sub>2</sub> twice. After the cell was heated to 50 °C (reaction temperature) by circulation of preheated oil outside the cell, CO<sub>2</sub> was introduced into it. The pressure was increased slowly while stirring by a Teflon-coated magnetic stirrer. When the pressure reached a certain value, the stirring was continued for 3–5 min and stopped; then, the state of the mixture including the substrate and CO<sub>2</sub> was visually examined. This examination was made at intervals of 0.2–0.5 MPa to determine the pressure at which the substrate was completely dissolved into CO<sub>2</sub>, forming a single phase. Then, the pressure was decreased in a similar way to determine the pressure at which droplets appeared (dew point), changing into a two-phase mixture. The pressures determined at increasing and decreasing pressures were less than  $\pm 0.3$  MPa different, and the average value of the two pressures determined was used. Those observations were used to estimate the solubility of benzaldehyde and cinnamaldehyde in CO<sub>2</sub> at different pressures.

**2.3. Hydrogenation of Aldehydes.** Hydrogenation of the two aldehydes in scCO<sub>2</sub> was carried out in a 50 cm<sup>3</sup> high-pressure



**Figure 1.** Estimated solubility of benzaldehyde in CO<sub>2</sub> and/or H<sub>2</sub> at 50 °C (open marks) along with the data of cinnamaldehyde at H<sub>2</sub> of 4 MPa (closed mark); for comparison, see ref 9.

stainless steel reactor. The reactor was charged with reactant and catalyst and then sealed. It was flushed with CO<sub>2</sub> three times and heated to 50 °C. After the introduction of H<sub>2</sub>, liquid CO<sub>2</sub> was introduced into the reactor with a high-pressure liquid pump to the desired pressure. The reaction was conducted while stirring the mixture with a magnetic stirrer for 2 h. The reactor was then cooled to room temperature with an ice bath and depressurized to atmospheric pressure. The reaction mixture was collected with acetone and analyzed with a gas chromatograph with a flame ionization detector. Previously, some authors reported that stainless steel reactors promoted chemical reactions such as hydrogenation and oxidation.<sup>29–31</sup> Hydrogenation reactions of benzaldehyde and cinnamaldehyde were conducted at pressures of 4 MPa H<sub>2</sub> and 10 MPa CO<sub>2</sub> in the absence of Pt/C catalyst. No products were observed to form with benzaldehyde, and a marginal quantity of hydrocinnamaldehyde was detected with cinnamaldehyde. Thus, the absence of reactor wall effects has been confirmed in the present cases.

**2.4. High-Pressure FTIR Measurements.** The information about interactions of dense CO<sub>2</sub> with the aldehydes dissolved at different pressures is significant in discussing the CO<sub>2</sub> effects during the reaction. In situ high-pressure FTIR spectra were measured at 50 °C with an FTIR spectrometer (FT/IR-620, JASCO) equipped with a 1.5 cm<sup>3</sup> high-pressure cell with a path length of 4 mm. The experimental procedure used is as follows: 10  $\mu$ L substrate, benzaldehyde or cinnamaldehyde, was added to the cell, it was heated to 50 °C by the circulation of preheated oil outside it, and H<sub>2</sub> and/or CO<sub>2</sub> was introduced into the cell. The pressure was raised slowly while stirring by a Teflon-coated magnetic stirrer. When the pressure reached a certain value, the stirring was continued for 3–5 min and stopped; then, the IR spectra were measured with a triglycine sulfate (TGS) detector at 4 cm<sup>-1</sup> wavenumber resolution by using pure CO<sub>2</sub> at the corresponding pressures as background.

## 3. Results and Discussion

**3.1. Phase Behavior and Solubility of Aldehydes.** The solubility of benzaldehyde in a mixture of CO<sub>2</sub> and H<sub>2</sub> was estimated from the phase behavior inspection at 50 °C in the same manner as that used for *trans*-cinnamaldehyde.<sup>9</sup> The results obtained are given in Figure 1, indicating that the solubility of benzaldehyde in pure CO<sub>2</sub> markedly increases with increasing CO<sub>2</sub> pressure at 9.8–11 MPa. At lower pressures, the quantity of benzaldehyde soluble in CO<sub>2</sub> was very small, and so, it was impossible to examine the phase behavior by visual inspection. Figure 1 also shows that the addition of H<sub>2</sub> significantly decreases the solubility of benzaldehyde, and this effect is larger

**TABLE 1: Influence of CO<sub>2</sub> Pressure on Benzaldehyde Hydrogenation with Pt/C Catalyst at 50 °C<sup>a</sup>**

entry	CO <sub>2</sub> pressure (MPa)	benzaldehyde conversion (%)	TOF <sup>b</sup> (s <sup>-1</sup> )	no. of phases
1	<i>c</i>	98	2.40	3
2	<i>d</i>	97	2.38	3
3	<i>e</i>	99	2.42	3
4	6.0	62	1.52	3
5	7.5	44	1.08	3
6	8.5	26	0.64	3
7	10.5	32	0.78	2
8	12.0	27	0.66	2
9	16.0	24	0.59	2

<sup>a</sup> Reaction conditions: benzaldehyde, 5 mmol; catalyst, 5% Pt/C, 10 mg (including Pt 2.56 μmol); H<sub>2</sub>, 4.0 MPa; reaction time, 2 h. <sup>b</sup> Turnover frequency, (moles of benzaldehyde reacted)/((moles of surface-exposed Pt atoms) × (reaction time)). The number of surface-exposed Pt atoms was calculated from the metal dispersion estimated from an approximate expression (see text). <sup>c</sup> In the absence of CO<sub>2</sub>. <sup>d,e</sup> In the presence of 6.0 and 10.1 MPa N<sub>2</sub>, respectively, instead of CO<sub>2</sub>.

at higher H<sub>2</sub> pressure, in accordance with the previous results for cinnamaldehyde.<sup>9</sup> The solubility of cinnamaldehyde determined previously at H<sub>2</sub> of 4 MPa is also given in Figure 1 for comparison, which is much smaller than that of benzaldehyde. Reaction conditions for hydrogenation were selected on the basis of these solubility data. The H<sub>2</sub> pressure of 4 MPa was used for hydrogenation reactions described in the following section.

**3.2. Influence of CO<sub>2</sub> Pressure on Benzaldehyde Hydrogenation.** The benzaldehyde hydrogenation was carried out at an H<sub>2</sub> pressure of 4.0 MPa and at different CO<sub>2</sub> pressures using 5.0 mmol benzaldehyde. Under these conditions, the reaction occurred in a three-phase system (CO<sub>2</sub>-rich gas, benzaldehyde-rich liquid, and catalyst solid phase) at CO<sub>2</sub> pressures below 10 MPa but in a two-phase system (CO<sub>2</sub>-rich gas and catalyst solid phase) at CO<sub>2</sub> pressures above 10.5 MPa. Table 1 gives the results obtained, in which the selectivity to benzyl alcohol is 100%. The total conversion of benzaldehyde merely decreases with CO<sub>2</sub> pressure up to 16 MPa. Under solvent (CO<sub>2</sub>)-free conditions, the reaction was almost completed in 2 h (entry 1), and this was not influenced by the presence of 6.0 and 10.1 MPa N<sub>2</sub> (entries 2, 3). In contrast, the use of 6.0 MPa CO<sub>2</sub> significantly decreased the conversion to 62% (entry 4). The conversion decreased with further increasing CO<sub>2</sub> pressure irrespective of the number of phases present, three or two phases. The highest conversion levels were obtained under solvent-less conditions and under pressurized N<sub>2</sub> atmosphere. Thus, dense CO<sub>2</sub> has only a negative effect on the hydrogenation of benzaldehyde, which is not the case for the hydrogenation of cinnamaldehyde as described below.

It should be noted here that the selectivity of benzyl alcohol is 100% in the presence of high-pressure CO<sub>2</sub> or N<sub>2</sub>, in contrast to the results in conventional organic solvents such as ethanol, in which toluene and/or benzene are also formed in about 10–20% as byproducts.<sup>32,33</sup>

Furthermore, the influence of CO<sub>2</sub> pressure was also examined under different conditions at which the hydrogenation took place in a two-phase system, using a certain amount of 5% Pt/C catalyst of 5.0 mg (including Pt 1.23 μmol). The CO<sub>2</sub> pressure was varied from 11 to 16 MPa while keeping the benzaldehyde/H<sub>2</sub>/CO<sub>2</sub> ratio unchanged (keeping the mole fraction of these species approximately unchanged) to minimize the influence of change of concentration of the reacting species on the reaction. For these experiments, we expected that the results did not include the influence of concentration change but did

**TABLE 2: Influence of CO<sub>2</sub> Pressure on Benzaldehyde Hydrogenation at 50 °C<sup>a</sup>**

entry	CO <sub>2</sub>		H <sub>2</sub>		benzaldehyde		conversion (%)
	MPa	mole fraction	MPa	mole fraction	mmol	mole fraction	
1	11	0.91	2.0	8.0 × 10 <sup>-2</sup>	3.0	6.4 × 10 <sup>-3</sup>	17
2	12	0.91	2.4	8.0	3.7	6.6	14
3	14	0.92	3.1	7.3	4.7	5.8	15
4	16	0.92	3.5	6.7	5.3	5.4	16

<sup>a</sup> Reaction conditions: 5% Pt/C catalyst, 5 mg (including Pt 1.23 μmol); reaction time, 2 h.

**TABLE 3: Influence of CO<sub>2</sub> Pressure on Cinnamaldehyde Hydrogenation with Pt/C Catalyst at 50 °C<sup>a</sup>**

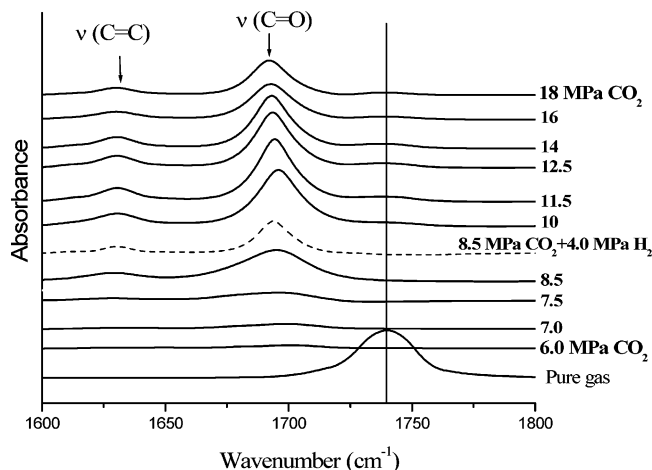
entry	CO <sub>2</sub> (MPa)	conversion (%)	selectivity <sup>b</sup> (%)			TOF (s <sup>-1</sup> )	no. phases
			COL	HCOL	HCAL		
1	<i>c</i>	32	77	10	13	0.78	3
2	<i>d</i>	36	71	19	10	0.89	3
3	<i>e</i>	38	67	18	15	0.92	3
4	6.0	38	80	14	6	0.93	3
5	7.5	42	82	12	6	1.02	3
6	8.5	47	81	9	10	1.15	3
7	10.5	55	80	9	11	1.35	2
8	12.0	38	78	9	13	0.93	2
9	16.0	36	80	7	13	0.88	2

<sup>a</sup> Reaction conditions: cinnamaldehyde, 0.25 mmol; catalyst, 5% Pt/C, 0.5 mg; H<sub>2</sub>, 4.0 MPa; time, 2 h. <sup>b</sup> COL: cinnamyl alcohol. HCOL: hydrocinnamyl alcohol. HCAL: hydrocinnamaldehyde. <sup>c</sup> In the absence of CO<sub>2</sub>. <sup>d,e</sup> In the presence of 6.0 and 9.7 MPa N<sub>2</sub>, respectively, instead of CO<sub>2</sub>.

include the influence of CO<sub>2</sub> pressure, if it existed, on the activity of the Pt/C catalyst. The latter was expected from one of our previous results in which the natures of fine metal particles changed in compressed CO<sub>2</sub> medium depending on the CO<sub>2</sub> pressure from optical absorption measurements with supported Au particles.<sup>21</sup> Table 2 indicates, however, that the conversion changes very little with the CO<sub>2</sub> partial pressure, and so, the specific activity of the Pt particles on the C support is unlikely to change significantly in the presence of dense CO<sub>2</sub>.

**3.3. Influence of CO<sub>2</sub> Pressure on Cinnamaldehyde Hydrogenation.** The hydrogenation of cinnamaldehyde was conducted under similar conditions as those used with benzaldehyde. Table 3 shows that the total conversion is 32% and the selectivity of cinnamyl alcohol is 77% under solvent (CO<sub>2</sub>)-free conditions (entry 1). The reaction was conducted under pressurized N<sub>2</sub> conditions at 6.0 and 9.7 MPa (entries 2, 3). It seems that the pressurization with N<sub>2</sub> increases the total conversion and decreases the selectivity of cinnamyl alcohol, while it decreases the selectivity of hydrocinnamaldehyde. However, these effects of N<sub>2</sub> are even less marked as compared with those observed under pressurized CO<sub>2</sub> conditions. The conversion and product distribution change significantly with increasing CO<sub>2</sub> pressure (entries 3–8), in contrast to the case of benzaldehyde. The conversion increased up to 55% at 10.5 MPa, at which the reaction system changed from a three-phase mixture to a two-phase mixture. At higher pressures, smaller conversions were obtained. The selectivity of cinnamyl alcohol was slightly improved in the presence of compressed CO<sub>2</sub>. Thus, the influence of CO<sub>2</sub> pressure observed in cinnamaldehyde hydrogenation is markedly different from that in benzaldehyde hydrogenation. The reasons for the difference in CO<sub>2</sub> pressure effects between these two substrates will be discussed later.

It is well-known that Pt is not a good catalyst for the selective hydrogenation of α,β-unsaturated aldehydes to unsaturated alcohols under ordinary conditions.<sup>34</sup> The selectivity may be

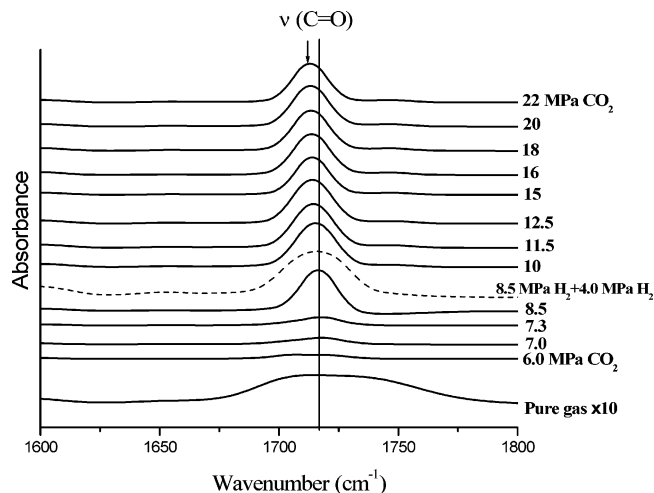


**Figure 2.** FTIR spectra of pure gaseous cinnamaldehyde and cinnamaldehyde dissolved in compressed CO<sub>2</sub> at 50 °C. Broken line is a spectrum in the presence of 4 MPa H<sub>2</sub> and 8.5 MPa CO<sub>2</sub>.

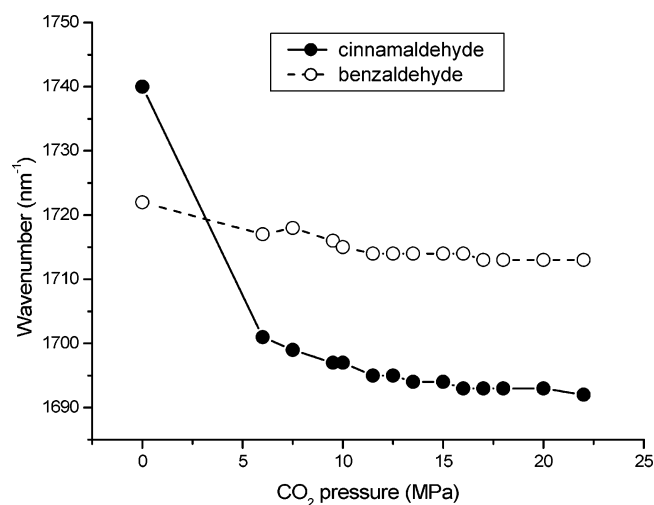
improved by alloying with other metal species such as tin. It is interesting that the selectivity of a Pt/C catalyst for the selective hydrogenation of cinnamaldehyde to cinnamyl alcohol can be improved when the reaction occurs under dense CO<sub>2</sub> conditions.

**3.4. Interactions between CO<sub>2</sub> and Aldehyde Molecules Measured by High-Pressure FTIR.** It is reported that interactions should exist between solutes and CO<sub>2</sub> molecules,<sup>24–27</sup> which would affect the reaction rate and product distribution in reactions in scCO<sub>2</sub>. So, high-pressure FTIR was used to examine such interactions in our reaction systems with cinnamaldehyde and benzaldehyde. Figure 2 gives FTIR spectra from 1800 to 1600 cm<sup>-1</sup> for the former substrate dissolved in compressed CO<sub>2</sub> at 50 °C. Gaseous cinnamaldehyde was examined as a reference, and its spectrum shows an absorption of ν(C=O) at 1740 cm<sup>-1</sup>. In compressed CO<sub>2</sub>, the spectra have strong ν(C=O) absorption and weak ν(C=C) absorption. The former absorption peak red-shifts to a smaller wavenumber with increasing CO<sub>2</sub> pressure compared with the gaseous substrate. This pressure effect on ν(C=O) is larger than that on ν(C=C). The results indicate the existence of interactions between cinnamaldehyde and dense CO<sub>2</sub> molecules, and these interactions are more significant for the C=O bond than the C=C bond. Figure 3 gives FTIR spectra for benzaldehyde, showing an absorption of ν(C=O) to red-shift in the presence of dense CO<sub>2</sub>. The extent of this red-shift is larger with increasing CO<sub>2</sub> pressure, but it is much smaller compared with the results of cinnamaldehyde, as clearly shown in Figure 4. The presence of 4 MPa H<sub>2</sub> does not change the peak position of ν(C=O) for both cinnamaldehyde and benzaldehyde, but the peak in the presence of H<sub>2</sub> is broader than that in the pure CO<sub>2</sub> for benzaldehyde. The results obtained from the FTIR measurements are summarized: A stronger interaction exists between CO<sub>2</sub> and cinnamaldehyde molecules than that between benzaldehyde and CO<sub>2</sub> molecules; the interaction with C=O of cinnamaldehyde is larger than that with C=C, and this interaction is not influenced by H<sub>2</sub> so much.

Moreover, the absorption of ν(C=O) in the CO<sub>2</sub> molecule was also examined. Figure 5 gives FTIR spectra obtained in the presence and absence of cinnamaldehyde and benzaldehyde in compressed CO<sub>2</sub>. The absorption peak of pure CO<sub>2</sub> is single at 1.5 MPa, but it splits into two peaks at higher pressures, indicating that CO<sub>2</sub> is not a nonpolar molecule in the supercritical region, although the net dipole moment of CO<sub>2</sub> is zero. The difference between these two peaks increases at increasing



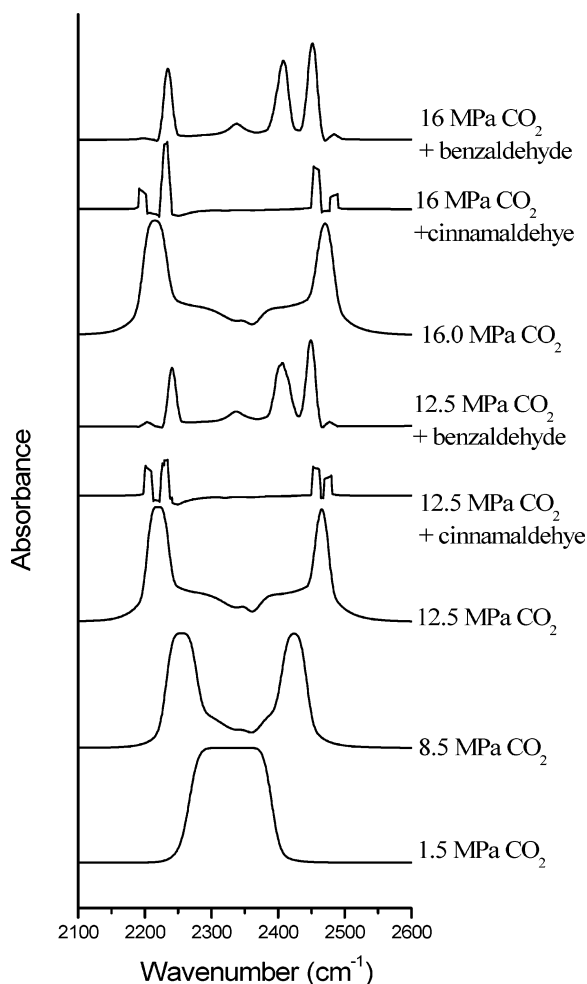
**Figure 3.** FTIR spectra of gaseous benzaldehyde and benzaldehyde dissolved in compressed CO<sub>2</sub> at 50 °C. Broken line is a spectrum in the presence of 4 MPa H<sub>2</sub> and 8.5 MPa CO<sub>2</sub>.



**Figure 4.** Influence of CO<sub>2</sub> pressure on the peak positions of ν(C=O) for cinnamaldehyde and benzaldehyde at 50 °C.

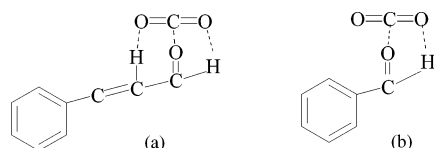
CO<sub>2</sub> pressure. Furthermore, note that these peaks split into four peaks in the presence of cinnamaldehyde at high CO<sub>2</sub> pressures of 12.5 and 16 MPa, while in the presence of benzaldehyde, one of the two peaks located at a larger wavenumber splits into two peaks. It is suggested that CO<sub>2</sub> molecules can interact with cinnamaldehyde and benzaldehyde molecules, but the modes of this interaction should be different between them.

In a CO<sub>2</sub> molecule, the carbon atom is partially positive and the oxygen atoms are partially negative. Thus, compressed CO<sub>2</sub> is not a nonpolar medium but a polar medium. In the literature, a specific interaction of CO<sub>2</sub> molecules with Lewis base groups, especially carbonyl groups, through a C—H···O hydrogen bond with the hydrogen atom attached to the carbonyl carbon or at the α-position has been reported.<sup>26</sup> Such hydrogen bonds for cinnamaldehyde can occur, while in the case of benzaldehyde having no hydrogen atom at the α-position, only one hydrogen bond can form with the hydrogen atom attached to carbonyl carbon. Possible interaction modes are illustrated in Scheme 1, which may explain the difference in the splitting of ν(C=O) absorption peaks in the presence of the two substrates (Figure 5). The two C=O bonds of a CO<sub>2</sub> molecule of configuration (a) are different from each other, and this may cause the second splitting in the presence of cinnamaldehyde at high CO<sub>2</sub> pressures. The two C=O bonds of a CO<sub>2</sub> molecule of config-



**Figure 5.** FTIR spectra of CO<sub>2</sub> at different pressures in the absence and presence of cinnamaldehyde and benzaldehyde at 50 °C.

**SCHEME 1: Possible Modes of Interaction of CO<sub>2</sub> with Cinnamaldehyde (a) or Benzaldehyde (b)**



uration (b) are also different, but the one bond may not be so different from the C=O bonds of the CO<sub>2</sub> molecules around this CO<sub>2</sub> molecule interacting with the carbonyl group. So, the second splitting should occur for the one peak only with benzaldehyde. The detail of the configuration of the CO<sub>2</sub> molecules nearest and second-nearest to a cinnamaldehyde or benzaldehyde molecule needs further investigation, in particular, theoretical modeling and calculation. The interaction of CO<sub>2</sub> with the carbonyl group of benzaldehyde should be weaker because of steric hindrance from the benzene ring, while such steric hindrance is not strong in cinnamaldehyde, because its carbonyl group is not located directly adjacent to the benzene ring. Nelson et al.<sup>25</sup> suggested that a specific interaction between CO<sub>2</sub> and the carbonyl oxygen could be described as a Lewis acid–base reaction; when a steric hindrance is present, the interaction of CO<sub>2</sub> and the carbonyl groups becomes weaker, resulting in a smaller degree of splitting of  $\nu(\text{C}=\text{O})$  of CO<sub>2</sub>, which is in agreement with our present results.

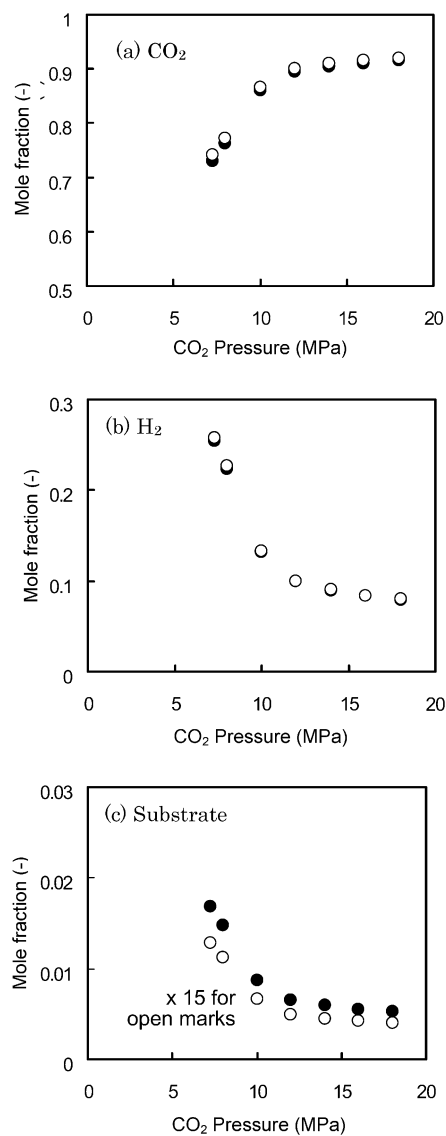
**3.5. Pressure Effects on Hydrogenation of Aldehydes in Dense CO<sub>2</sub>.** As described above, the conversion of benzaldehyde simply decreases with CO<sub>2</sub> pressure, while the conversion

of cinnamaldehyde has a maximum at a certain CO<sub>2</sub> pressure (Tables 1 and 3). The possible effects, both positive and negative, of CO<sub>2</sub> pressure on the hydrogenation of aldehydes are as follows: (a) dilution of reacting species, (b) modification of the reactivity of the C=O bond, and (c) change of the specific activity of catalyst.

In the case of benzaldehyde, (b) is insignificant from FTIR results and (c) is not significant for the present catalyst used (Table 2). In the experiments of Table 2, the relative quantities of benzaldehyde, H<sub>2</sub>, and CO<sub>2</sub> are approximately the same even at different CO<sub>2</sub> pressures. Under these conditions, the influence of the concentration (mole fraction) of reacting species on the conversion of benzaldehyde was insignificant, and we expected to consider independently the influence of CO<sub>2</sub> pressure on the activity of supported Pt particles. On the basis of the results of Tables 1 and 2, we may say that compressed CO<sub>2</sub> does not have a positive effect on enhancement of the catalytic activity. Thus, (a) is the main reason for the simple decrease in the benzaldehyde conversion with CO<sub>2</sub> pressure. At high pressures, there are a CO<sub>2</sub>-rich gas phase, in which all benzaldehyde is soluble, and a catalyst solid phase. Increasing the CO<sub>2</sub> pressure merely decreases the concentration of the substrate in the gas phase, resulting in a decrease in the conversion (simple dilution effect). The situation is not simple at low pressures, because the reaction may occur in the benzaldehyde liquid phase and in the CO<sub>2</sub>-rich gas phase. When the CO<sub>2</sub> pressure is raised, more benzaldehyde is soluble in the gas phase and more CO<sub>2</sub> and H<sub>2</sub> are soluble in the liquid phase. The solubility of benzaldehyde in the gas phase at low pressures is very small (Figure 1), and so, the reaction is likely to occur mainly in the liquid phase. The dilution of benzaldehyde with dissolved CO<sub>2</sub> and H<sub>2</sub> should be responsible for the decrease in the conversion with CO<sub>2</sub> pressure at low pressures as well.

Next, we will consider (a) and (b) in the case of cinnamaldehyde hydrogenation. The reaction is also likely to occur in the cinnamaldehyde liquid phase at low CO<sub>2</sub> pressures for the same reasons as already mentioned for benzaldehyde. When the CO<sub>2</sub> pressure is raised, the concentration of H<sub>2</sub> in the liquid phase increases because of the dissolution of CO<sub>2</sub>, and in addition, the C=O bond of cinnamaldehyde becomes more reactive through interactions with the CO<sub>2</sub> molecule (red-shift increases with CO<sub>2</sub> pressure as illustrated in Figures 2 and 4), resulting in the enhancement of cinnamaldehyde conversion as observed (Table 3). At elevated pressures producing a two-phase mixture, the reaction occurs in a CO<sub>2</sub>-gas phase, causing the decrease in the conversion with CO<sub>2</sub> pressure due to the simple dilution effects.

The mole fractions of substrates, H<sub>2</sub>, and CO<sub>2</sub> in the reaction mixture were estimated at different CO<sub>2</sub> pressures by a simple calculation. Moles of pure H<sub>2</sub> and CO<sub>2</sub> were calculated by an equation of state,  $PV = ZnRT$ ; the compressibility factor  $Z$  was assumed to be unity for H<sub>2</sub>, while it was determined as a function of pressure for CO<sub>2</sub>.<sup>35</sup> From the moles of pure components determined, the mole fraction was then calculated under the reaction conditions. The results calculated are plotted against CO<sub>2</sub> pressure in Figure 6. The reaction mixture includes liquid and gas phases (in addition to catalyst solid phase) at low pressures, and so, the results are average values within the reactor. At high pressures above 10 MPa, the reaction mixture is a single gas phase, and the concentrations of substrates and H<sub>2</sub> significantly decrease with CO<sub>2</sub> pressure. This should be responsible for the decrease observed in the conversion of hydrogenation of cinnamaldehyde and benzaldehyde at elevated pressures.



**Figure 6.** Mole fraction of substrates, H<sub>2</sub>, and CO<sub>2</sub> as a function of CO<sub>2</sub> pressure for benzaldehyde–H<sub>2</sub>–CO<sub>2</sub> (closed marks) and cinnamaldehyde–H<sub>2</sub>–CO<sub>2</sub> (open marks) reaction systems under hydrogenation conditions. Substrate benzaldehyde, 0.25 mmol; cinnamaldehyde, 5.0 mmol; H<sub>2</sub>, 4 MPa; temperature, 50 °C.

#### 4. Conclusion

The influence of CO<sub>2</sub> pressure in the hydrogenation of benzaldehyde is significantly different from that of cinnamaldehyde. There are interactions of compressed CO<sub>2</sub> molecules with these two aldehydes. The mode and strength of the interactions are different, and the C=O bond of cinnamaldehyde becomes more reactive, but this promotion effect is less significant with benzaldehyde. Thus, the conversion of benzaldehyde hydrogenation simply decreases with CO<sub>2</sub> pressure because of a dilution effect, while that of cinnamaldehyde hydrogenation has a maximum at a certain pressure depending

on the activation of the C=O bond at low pressures and the simple dilution at higher pressures. The specific activity of the Pt/C catalyst is unlikely to be enhanced in the presence of dense CO<sub>2</sub>.

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#### References and Notes

- Baiker, A. *Chem. Rev.* **1999**, *99*, 453–473.
- Jessop, G.; Leitner, W., Eds. *Chemical Synthesis Using Supercritical Fluids*; Wiley-VCH: Weinheim, 1999.
- Oakes, S.; Clifford, A. A.; Rayner, C. M. *J. Chem. Soc., Perkin Trans. 1* **2001**, 917–941.
- Beckman, E. J. *J. Supercrit. Fluids* **2003**, *60*, 815–833.
- Banet Osuna, A. M.; Chen, W.; Hope, E. G.; Kemmitt, R. D. W.; Paige, D. R.; Stuart, A. M.; Xiao, J.; Xu, L. *J. Chem. Soc., Dalton Trans.* **2000**, 4052–4055.
- Palo, D. R.; Erkey, C. *Organometallics* **2000**, *19*, 81–86.
- Koch, D.; Leitner, W. *J. Am. Chem. Soc.* **1998**, *120*, 13398–13404.
- Fujita, S.; Fujisawa, S.; Bhanage, B. M.; Ikushima, Y.; Arai, M. *Eur. J. Org. Chem.* **2004**, 2881–2887.
- Zhao, F.; Ikushima, Y.; Chatterjee, M.; Sato, O.; Arai, M. *J. Supercrit. Fluids* **2003**, *27*, 65–72.
- Phiong, H.-S.; Lucien, F. P.; Adesina, A. A. *J. Supercrit. Fluids* **2003**, *25*, 155–164.
- Tschan, R.; Wandeler, R.; Schneider, M. S.; Schubert, M. M.; Baiker, A. *J. Catal.* **2001**, *204*, 219–229.
- Zhao, F.; Ikushima, Y.; Chatterjee, M.; Shirai, M.; Arai, M. *Green Chem.* **2003**, *5*, 76–79.
- Zhao, F.; Ikushima, Y.; Arai, M. *J. Catal.* **2004**, *224*, 479–483.
- Zhao, F.; Zhang, R.; Chatterjee, M.; Ikushima, Y.; Arai, M. *Adv. Synth. Catal.* **2004**, *346*, 661–668.
- Zhao, F.; Ikushima, Y.; Shirai, M.; Ebina, T.; Arai, M. *J. Mol. Catal. A: Chem.* **2002**, *180*, 259–265.
- Bhanage, B. M.; Ikushima, Y.; Shirai, M.; Arai, M. *Catal. Lett.* **1999**, *62*, 175–177.
- Chouchi, D.; Gourgouillon, D.; Courel, M.; Vital, J.; Ponte, M. N. *Ind. Eng. Chem. Res.* **2001**, *40*, 2551–2554.
- Jenzer, G.; Schneider, M. S.; Wandeler, R.; Mallat, T.; Baiker, A. *J. Catal.* **2001**, *199*, 141–148.
- Hitzler, M. G.; Smail, F. R.; Ross, S. K.; Poliakoff, M. *Org. Process Res. Dev.* **1998**, *2*, 137–146.
- Ross, S. K.; Meehan, N. J.; Poliakoff, M.; Carter, D. U.K. Patent GB 2,374,071A, 2002; p 12.
- Arai, M.; Nishiyama, Y.; Ikushima, Y. *J. Supercrit. Fluids* **1998**, *13*, 149–153.
- Leitner, W. *Coordin. Chem. Rev.* **1996**, *153*, 257–284.
- Walther, D.; Ruben, M.; Rau, S. *Coordin. Chem. Rev.* **1999**, *182*, 67–100.
- Hyatt, J. A. *J. Org. Chem.* **1984**, *49*, 5097–5101.
- Nelson, M. R.; Brokman, R. F. *J. Phys. Chem. A* **1998**, *102*, 7860–7863.
- Raveendran, P.; Wallen, S. L. *J. Am. Chem. Soc.* **2002**, *124*, 12590–12599.
- Grunwaldt, J.-D.; Wandeler, R.; Baiker, A. *Catal. Rev.—Sci. Eng.* **2003**, *45*, 1–96.
- Boudart, M.; Djega-Mariadassou, G. *Kinetics of Heterogeneous Catalytic Reaction*; Princeton University Press: Princeton, NJ, 1984.
- Loeker, F.; Leitner, W. *Chem.—Eur. J.* **2000**, *6*, 2011–2015.
- Ranu, B. C.; Dey, S. S.; Hajra, A. *Green Chem.* **2003**, *5*, 44–46.
- Zhao, F.; Ikushima, Y.; Arai, M. *Green Chem.* **2003**, *5*, 656–658.
- Vannice, M. A.; Poondi, D. *J. Catal.* **1998**, *178*, 386–390.
- Pinna, F.; Menegazzo, F.; Signoretto, M.; Canton, P.; Fagherazzi, G.; Pernicone, N. *Appl. Catal., A* **2001**, *219*, 195–200.
- Gallezot, P.; Richard, D. *Catal. Rev.—Sci. Eng.* **1998**, *40*, 81–126.
- Smith, J. M.; Van Ness, H. C. *Introduction to Chemical Engineering Thermo-dynamics*; McGraw-Hill: New York, 1975.